

## Exercise

5A.2(b) Let A stand for water and B for  $\text{MgSO}_4(\text{aq})$

$$V_J = \left( \frac{\partial V}{\partial n_J} \right)_{p,T,n'} \quad [5A.1] = \left( \frac{dv}{dx} \right) \left( \frac{dV}{dv} \right) \left( \frac{\partial x}{\partial n_J} \right)_{n'}$$

$$\text{Now } x = \frac{b}{b^\ominus} = \frac{n_B}{n_A M_A b^\ominus} \quad \text{so} \quad \left( \frac{\partial x}{\partial n_B} \right)_{n_A} = \frac{1}{n_A M_A b^\ominus}$$

$$\text{and } V_B = 2 \times 34.69 \times (x - 0.070) \frac{\text{cm}^3}{n_A M_A b^\ominus}$$

Evaluate this expression for  $b = 0.050 \text{ mol kg}^{-1}$  ( $x = 0.050$ ), recalling that the original expression for  $v$  applies for 1.000 kg of water (*i.e.*, for  $n_A M_A = 1.000 \text{ kg}$ ). The result is  $V_B = \boxed{-1.4 \text{ cm}^3 \text{ mol}^{-1}}$ .

The total volume consisting of 0.050 mol of  $\text{MgSO}_4$  and 1.000 kg (55.49 mol) water is

$$V = 1001.21 + 34.69 \times (0.050 - 0.070) = 1001.23 \text{ cm}^3.$$

The total volume is also equal to

$$V = V_A n_A + V_B n_B \quad [5A.3].$$

$$\text{Therefore, } V_A = \frac{V - V_B n_B}{n_A} = \frac{1001.21 \text{ cm}^3 - (-1.4 \text{ cm}^3) \times (0.050 \text{ mol})}{55.49 \text{ mol}} = \boxed{18.04 \text{ cm}^3 \text{ mol}^{-1}}$$

5A.4(b) The Gibbs energy of mixing perfect gases is

$$\Delta_{\text{mix}} G = nRT(x_A \ln x_A + x_B \ln x_B) \quad [5A.16] = pV(x_A \ln x_A + x_B \ln x_B) \quad [\text{perfect gas law}]$$

Because the compartments are of equal size, each contains half of the gas; therefore,

$$\Delta_{\text{mix}} G = (pV) \times \left( \frac{1}{2} \ln \frac{1}{2} + \frac{1}{2} \ln \frac{1}{2} \right) = -pV \ln 2$$

$$= -(100 \times 10^3 \text{ Pa}) \times (250 \text{ cm}^3) \left( \frac{1 \text{ m}^3}{10^6 \text{ cm}^3} \right) \times \ln 2 = -17.3 \text{ Pa m}^3 = \boxed{-17.3 \text{ J}}$$

$$\Delta_{\text{mix}} S = -nR(x_A \ln x_A + x_B \ln x_B) \quad [5A.17] = \frac{-\Delta_{\text{mix}} G}{T} = \frac{+17.3 \text{ J}}{273 \text{ K}} = \boxed{+0.635 \text{ J K}^{-1}}$$

5A.8(b) Let W denote water and E ethanol. The total volume of the solution is

$$V = n_W V_W + n_E V_E$$

We are given  $V_E$ , we need to determine  $n_W$  and  $n_E$  in order to solve for  $V_W$ , for

$$V_W = \frac{V - n_E V_E}{n_W}$$

Take  $100 \text{ cm}^3$  of solution as a convenient sample. The mass of this sample is

$$m = \rho V = (0.9687 \text{ g cm}^{-3}) \times (100 \text{ cm}^3) = 96.87 \text{ g}.$$

80 per cent of this mass water and 20 per cent ethanol, so the moles of each component are

$$n_W = \frac{(0.80) \times (96.87 \text{ g})}{18.02 \text{ g mol}^{-1}} = 4.3 \text{ mol} \quad \text{and} \quad n_E = \frac{(0.20) \times (96.87 \text{ g})}{46.07 \text{ g mol}^{-1}} = 0.42 \text{ mol}^{-1}.$$

$$V_W = \frac{V - n_E V_E}{n_W} = \frac{100 \text{ cm}^3 - (0.42 \text{ mol}) \times (52.2 \text{ cm}^3 \text{ mol}^{-1})}{4.3 \text{ mol}} = \boxed{18 \text{ cm}^3 \text{ mol}^{-1}}$$

**5B.1(b)** In Exercise 5A.10(b), the Henry's law constant was determined for concentrations expressed in mole fractions;  $K_B = 8.2 \times 10^3$  kPa. Thus the concentration must be converted from molality to mole fraction

$$m_A = 1000 \text{ g, corresponding to } n_A = \frac{1000 \text{ g}}{74.1 \text{ g mol}^{-1}} = 13.50 \text{ mol}$$

$$\text{Therefore } x_B = \frac{0.25 \text{ mol}}{(0.25 \text{ mol}) + (13.50 \text{ mol})} = 0.018$$

The pressure is

$$p_B = K_B x_B [5A.23] = (0.018) \times (8.2 \times 10^3 \text{ kPa}) = \boxed{1.5 \times 10^2 \text{ kPa}}.$$

**5B.6(b)** (i) Benzene and ethylbenzene form nearly ideal solutions, so.

$$\Delta_{\text{mix}} S = -nRT(x_A \ln x_A + x_B \ln x_B) [5A.17]$$

We need to differentiate eqn 5A.17 with respect to  $x_A$  and look for the value of  $x_A$  at which the derivative is zero. Since  $x_B = 1 - x_A$ , we need to differentiate

$$\Delta_{\text{mix}} S = -nRT\{x_A \ln x_A + (1-x_A)\ln(1-x_A)\}$$

This gives (using  $\frac{d \ln x}{dx} = \frac{1}{x}$ )

$$\frac{d\Delta_{\text{mix}} S}{dx_A} = -nR\{\ln x_A + 1 - \ln(1-x_A) - 1\} = -nR \ln \frac{x_A}{1-x_A}$$

which is zero when  $x_A = \frac{1}{2}$ . Hence, the maximum entropy of mixing occurs for the preparation of a mixture that contains equal mole fractions of the two components.

(ii) Because entropy of mixing is maximized when  $n_E = n_B$  (changing to notation specific to Benzene and Ethylbenzene)

$$\frac{m_E}{M_E} = \frac{m_B}{M_B}$$

This makes the mass ratio

$$\frac{m_B}{m_E} = \frac{M_B}{M_E} = \frac{78.11 \text{ g mol}^{-1}}{106.17 \text{ g mol}^{-1}} = \boxed{0.7357}$$

**5B.7(b)** The ideal solubility in terms of mole fraction is given by eqn 5B.15:

$$\begin{aligned} \ln x_{\text{Pb}} &= \frac{\Delta_{\text{fus}} H}{R} \times \left( \frac{1}{T_f} - \frac{1}{T} \right) \\ &= \left( \frac{5.2 \times 10^3 \text{ J mol}^{-1}}{8.3145 \text{ J K}^{-1} \text{ mol}^{-1}} \right) \times \left( \frac{1}{600. \text{ K}} - \frac{1}{553 \text{ K}} \right) = -0.089 \end{aligned}$$

Therefore,  $x_{\text{Pb}} = e^{-0.089} = 0.92$ .

$$x_{\text{Pb}} = \frac{n_{\text{Pb}}}{n_{\text{Bi}} + n_{\text{Pb}}} \quad \text{implying that} \quad n_{\text{Pb}} = \frac{n_{\text{Bi}} x_{\text{Pb}}}{1 - x_{\text{Pb}}} = \frac{m_{\text{Bi}}}{M_{\text{Bi}}} \times \frac{x_{\text{Pb}}}{1 - x_{\text{Pb}}}$$

Hence the amount of lead that dissolves in 1 kg of bismuth is

$$n_{\text{Pb}} = \frac{1000 \text{ g}}{209 \text{ g mol}^{-1}} \times \frac{0.92}{1 - 0.92} = \boxed{52 \text{ mol}}$$

or, in mass units,  $m_{\text{Pb}} = n_{\text{Pb}} \times M_{\text{Pb}} = 52 \text{ mol} \times 207 \text{ g mol}^{-1} = 1.1 \times 10^4 \text{ g} = \boxed{11 \text{ kg}}$ .

**5B.9(b)** In an ideal dilute solution the solvent ( $\text{CCl}_4$ , A) obeys Raoult's law [5A.21] and the solute ( $\text{Br}_2$ , B) obeys Henry's law [5A.23]; hence

$$p_A = x_A p_A^* = (0.934) \times (23 \text{ kPa}) = \boxed{21.5 \text{ kPa}}$$

$$p_B = x_B K_B = (0.066) \times (73 \text{ kPa}) = \boxed{4.8 \text{ kPa}}$$

$$p_{\text{total}} = (21.5 + 4.8) \text{ kPa} = \boxed{26.3 \text{ kPa}}$$

The composition of the vapour in equilibrium with the liquid is

$$y_A = \frac{p_A}{p_{\text{total}}} = \frac{21.5 \text{ kPa}}{26.3 \text{ kPa}} = \boxed{0.82} \quad \text{and} \quad y_B = \frac{p_B}{p_{\text{total}}} = \frac{4.8 \text{ kPa}}{26.3 \text{ kPa}} = \boxed{0.18}$$

**5B.13(b)** (i) If the solution is ideal, then the partial vapour pressures are given by Raoult's law [5A.21]:

$$p_B = x_B p_B^* = 0.50 \times 9.9 \text{ kPa} = 4.95 \text{ kPa}$$

$$p_T = x_T p_T^* = 0.50 \times 2.9 \text{ kPa} = 1.45 \text{ kPa}$$

The total pressure is

$$p_{\text{total}} = p_B + p_T = (4.95 + 1.45) \text{ kPa} = \boxed{6.4 \text{ kPa}}.$$

(ii) The composition of the vapour is given by

$$y_B = \frac{p_B}{p_{\text{total}}} = \frac{4.95 \text{ kPa}}{6.4 \text{ kPa}} = \boxed{0.77}$$

$$\text{and} \quad y_T = \frac{p_T}{p_{\text{total}}} = \frac{1.45 \text{ kPa}}{6.4 \text{ kPa}} = \boxed{0.23}$$

(iii) When only a few drops of liquid remain, the equimolar mixture is almost entirely vapour. Thus  $y_B = y_T = 0.50$ , which implies that

$$p_B = x_B p_B^* = p_T = x_T p_T^* = (1 - x_B) p_T^*.$$

Solving for  $x_B$  yields

$$x_B = \frac{p_T^*}{p_B^* + p_T^*} = \frac{2.9 \text{ kPa}}{(9.9 + 2.9) \text{ kPa}} = 0.23$$

The partial vapour pressures are

$$p_B = x_B p_B^* = 0.23 \times 9.9 \text{ kPa} = 2.24 \text{ kPa} = p_T \text{ [vapour mixture is equimolar]} = p_{\text{total}}/2.$$

The total pressure is

$$p_{\text{total}} = 2p_B = \boxed{4.5 \text{ kPa}}.$$

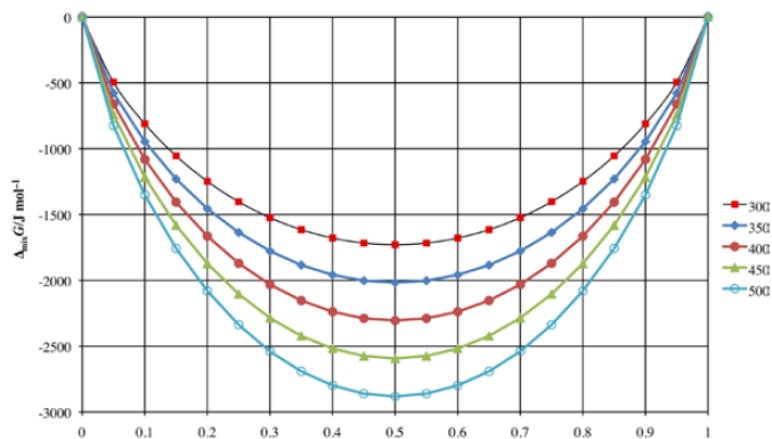
## Problem

**5B.12** The Gibbs energy of mixing an ideal solution is [5A.16]

$$\Delta_{\text{mix}}G = nRT(x_A \ln x_A + x_B \ln x_B)$$

The molar Gibbs energy of mixing is plotted against composition for several temperatures in Fig. 5B.4. The legend shows the temperature in kelvins.

**Figure 5B.4**



The composition at which the temperature dependence is strongest is the composition at which the function has its largest magnitude, namely  $x_A = x_B = 0.5$ .